

AMENDMENTS TO THE SPECIFICATION

On page 1, please replace the second full paragraph with the following amended paragraph:

More especially, the invention relates to a method for the industrial concentration of substantially liquid mixtures and solutions within all industrial sectors, such as, for example, the food sector, and in the disposal of urban refuse, in purification plants, and in the recovery of heavy metals contained in aqueous solutions, etc.[.]

On page 2, please replace the first full paragraph with the following amended paragraph:

The first type of technology comprises a series arrangement of two or more concentrators each comprising a container filled with the mixture to be concentrated, a coil heating device which is immersed in the liquid mixture and which is generally fed with steam, and finally a pipe system which connects in series the two or more containers constituting the plant. The liquid mixture in the first container is heated and concentrated by means of mains steam. After having reached a specific degree of concentration, the liquid mixture is conveyed into the next container where it is subjected to an analogous treatment, the only difference being that, in this case, the mains steam is replaced by the [[vapour]] vapor coming from the first container, or that released from the liquid mixture in the first concentration stage. The process just described can be repeated several times until the desired concentration is obtained.

On pages 2-3, please replace the bridging paragraph with the following amended paragraph:

With this type of technology, however, it is possible to reach only a specific degree of concentration, which is determined by the viscosity of the product to be treated, because it is

necessary to ensure that the product, which becomes gradually more dense, runs well from one container to another in the concentration plant in order to avoid undesired obstructions in the connecting pipe system. This problem is further aggravated if the liquid mixture to be treated contains various types of [[fibre]] fiber, or aggregates of insoluble salts or the like. A further disadvantage presented by any type of liquid mixture to be treated, however, is that of the encrustations which form on the heating coils which have to be dismounted and cleaned periodically.

On page 3, please replace the first full paragraph with the following amended paragraph:

The second type of apparatus, the vacuum concentrators, normally comprise a container heated by a jacket or a heating coil, the latter being immersed in the liquid mixture to be treated, and a condenser for condensing the [[vapour]] vapor formed in the concentration stage.

On page 6, please replace the second full paragraph with the following amended paragraph:

Advantageously, a stream of hot dry air is fed into the turbo-concentrator in the same direction as the stream of liquid mixture; thus, the speed at which [[vapour]] vapor is removed is increased, which further reduces the residence times necessary for the stream in the concentration unit.

Please delete the present Abstract of the Disclosure and replace it with the following amended Abstract of the Disclosure (a replacement Abstract of the Disclosure which can be substituted into the application is attached hereto).

A method for the concentration of liquid mixtures[, comprising] includes the step of causing a continuous stream of the liquid mixtures to flow in the form of a turbulent thin layer in contact with a heated wall; for that purpose, a continuous stream of liquid mixture is fed into a turbo-concentrator [[comprising]] including a cylindrical tubular body (1), a heating jacket (4) and a bladed rotor (8) rotatably supported in the cylindrical tubular body (1), and is centrifuged to form a dynamic and tubular thin layer, the thin layer advancing inside the cylindrical tubular body (1) then being discharged continuously in the form of a stream of concentrated liquid mixture.